Performance Investigation of a Three-Bed Adsorption Chiller With and Without Mass Recovery

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Abstract— In this paper, the performance of a three-bed (equal bed) adsorption chiller with and without mass recovery has been numerically studied. Silica gel-water is chosen as adsorbent-refrigerant pair. The three-bed adsorption chiller comprises with three adsorber/desorber heat exchanger, one evaporator and one condenser. In the present numerical solution, the heat source temperature variation is taken from 50°C to 65°C along with coolant inlet temperature at 30°C and the chilled water inlet temperature at 14°C. In the present strategy, mass recovery process occurs in all bed. The configuration of beds in the three-bed chiller with mass recovery were taken as uniform in size. The performances in terms of cooling capacity (CC) and coefficient of performance (COP) are compared with those of conventional three-bed without mass recovery scheme. Results show that three-bed with mass recovery scheme provides more CC values than those provided by the three-bed system without mass recovery scheme while it provides better COP values for 65°C heat source temperature.

Keywords*:* Adsorption Chiller, Silica gel-water, Mass recovery, Renewable energy sources, CC, COP, Chiller efficiency

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1. INTRODUCTION

Most of the advanced cycles in adsorption refrigeration/heat pump are proposed to achieve high Coefficient of Performance (COP) and/or Cooling Capacity (CC) values. Few cycles, however, are proposed to utilize relatively low temperature heat source. Saha et al. [1] proposed two-stage chiller where the driving heat source temperature was validated experimentally. Khan et al.[2] studied the performance investigation on mass recovery three-bed adsorption cycle. Later, Khan et al.[3] proposed and investigated numerically the advanced three-bed adsorption chiller employing mass recovery scheme. Saha et al.[4] studied waste heat driven dual-mode, multi-stage, multi-bed regenerative adsorption system.

To improve the coefficient of performance, Shelton et al. [5] proposed a thermal wave regenerative adsorption heat pump system. Wang [6] showed that mass recovery process is very effective for the high evaporating pressure lift as well as for the low regenerating temperature. Alam et al. [7] analyzed four-bed mass recovery cycle with silica gel/water pair employing a new strategy to improve the cooling effect. Recently, Sahaet al.[8] analyzed a dual-mode, multi-bed adsorption chiller to improve the heat recovery efficiency.

The primary objective of the study is to determine the numerical result of a three-bed (equal bed) adsorption chiller with and without mass recovery. A cycle simulation computer program is constructed to analyze the influence of operating conditions (hot and cooling water temperature) on COP (Coefficient of Performance), CC (Cooling Capacity) and chilled water outlet temperature.

2. WORKINGPRINCIPLEOF THE MASS RECOVERY CHILLER

The schematic diagram and time allocation of the proposed three-bed mass recovery chiller are shown in Fig. 1 and Table 1, respectively. The three-bed mass recovery chiller comprises with three sorption elements (adsorber/desorber heat exchangers), a condenser, an evaporator, and metallic tubes for hot, cooling and chilled water flows as shown in Fig.

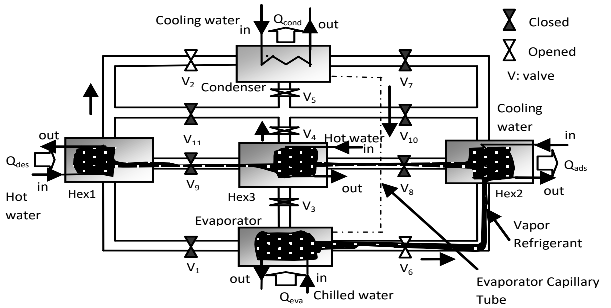
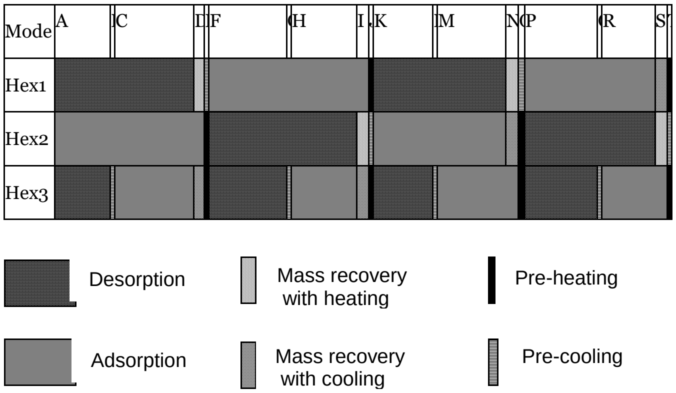


Fig. 1.Schematic of three bed chiller with mass recovery (Proposed Cycle)

Operational strategy of the proposed chiller is shown in Table.1. In proposed design, mass recovery process occurs in all bed. To complete a full cycle for the proposed system, the chiller needs 20modes, namely A,B,C,D,E, F,G,H, I, J, K, L, M, N,O ,P, Q, R, S and T as can be seen from Table 1.

TABLE 1
OPERATIONAL STRATEGY OF THE THREE BED CHILLER WITH MASS RECOVERY



In mode A, Hex1 and Hex3 work as desorber. The desorption-condensation process takes place at condenser pressure (P_{cond}). The desorber (Hex1, Hex3) is heated up to temperature (T_{des}) by heat input $Q_{des,}$ provided by the driving heat sources. The resulting refrigerant is cooled down by temperature (T_{cond}) in the condenser by the cooling water, which removes condensation heat, $Q_{cond.}$ Hex2 works as adsorber in mode A. In the adsorption-evaporation process, refrigerant (water) in evaporator is evaporated at evaporation temperature, $T_{eva,}$ and seized heat, Q_{eva} from chilled water. The evaporated vapor is adsorbed by adsorbent (silica gel), at which cooling water removes the adsorption heat, $Q_{ads.}$ Mode B is the pre-cooling process for Hex3.In pre-cooling process, Hex3 is isolated from evaporator, condensed or any other beds. Cooling water is supplied to the bed for short time (30s) in this period. Hex1 works as desorber and Hex2 works as adsorber in mode B also. Mode C is the adsorption process for Hex3, Hex2 and desorption process for Hex1. In mode D,Hex3 (at the end position of adsorption-evaporation process) and Hex1 (at the end position of desorption-condensation process) are connected with each other continuing cooling water and hot water, respectively that can be classified as two-bed mass recovery process. This time Hex3 is isolated from evaporated and Hex1 is isolated from condensed. Here mass recovery occurs only bed to bed. In this mode Hex2 works as adsorber. When the concentration levels of both beds Hex1 and Hex3 reach in nearly equilibrium levels, then warm up process will start, called mode E (pre-heating or pre-cooling).

In mode E, Hex2 and Hex3 are heated up by hot water, and Hex1 is cooled down by cooling water. When the pressure of Hex2 and Hex3 are nearly equal to the pressure of condenser then Hex2 and Hex3 are connected to condenser. When the pressure of Hex1 is nearly equal to the pressure of evaporator then Hex1 is connected to evaporator. In mode F, Hex2 and Hex3 work as desorber and Hex1 works as adsorber. Mode G is the pre-cooling process for Hex3. In this mode, Hex2 works as desorber and Hex1 works as adsorber. Mode H is the adsorption-evaporation process for Hex1 and Hex3. Hex2 works as desorber in this mode. In mode I,Hex3 (at the end position of adsorption-evaporation process) and Hex2 (at the end position of desorption-condensation process) are connected with each other continuing cooling water and hot water, respectively that can be classified as two-bed mass recovery process. When the concentration levels of both beds Hex3 and Hex2 reach in nearly equilibrium levels, then warm up process will start, called mode J (pre-heating or pre-cooling). Hex1 works as adsorber in this mode. Mode J is the pre-heating/pre-cooling process for all bed. In this period, Hex1 and Hex3 are heated up by hot water; Hex2 is cooled down by cooling water. Modes K, L and Mare same as modes A, B and C respectively. In mode K, L and M Hex1 and Hex3 work as desorber and Hex2 works as adsorber. The mode N is same as mode D. In these modes, Hex2 (at the end position of adsorption-evaporation process) and Hex1 (at the end position of desorption-condensation process) are connected with each other continuing cooling water and hot water respectively. In this mode Hex3 works as adsorber. When the concentration levels of both beds Hex1 and Hex2 reach in nearly equilibrium levels, then warm up process will start, called mode O (pre-heating or pre-cooling). The mode O is same as mode E. Modes P, Q and R are same as modes F, G and H respectively. In mode P, Q and R, Hex2 and Hex3 work as desorber and Hex1 works as adsorber. The mode S is same as mode I. In mode S, Hex1 (at the end position of adsorption-evaporation process) and Hex2 (at the end position of desorption-condensation process) are connected with each other continuing cooling water and hot water, respectively that can be classified as two-bed mass recovery process. When the concentration levels of both beds Hex1 and Hex2 reach in nearly equilibrium levels, then warm up process will start, called mode T (pre-heating or pre-cooling). Hex3 works as adsorber in this mode. Mode T is the pre-heating/pre-cooling process for all bed. In this period, Hex1 and Hex3 are heated up by hot water; Hex2 is cooled down by cooling water. Mode T is the last process for all beds, after this mode, all beds will return to its initial position (Mode A). That's why to complete one cycle, it needs 20 modes.

3. MATHEMATICAL FORMULATION

The heat transfer and energy balance equations for the adsorbent bed can be described as follows:

$$T_{w,\,out}=T_{hex}+\left(T_{w,\,in}-T_{hex}\right)\exp\left(-\frac{U_{hex}A_{hex}}{\dot{m}_w C_{pw}}\right) \qquad (1)$$

$$\frac{d}{dt}\left\{\left(W_s\left(C_{ps}+C_{pw}q\right)+W_{khex}C_{pcu}+W_{fhex}C_{pAl}\right)T_{hex}\right\}=W_s Q_{st}\frac{dq}{dt}$$
$$-\delta W_s C_{pw}\left\{\gamma\left(T_{hex}-T_{eva}\right)+\left(1-\gamma\right)\left(T_{hex}-T_{wv}\right)\right\}\frac{dq}{dt} \qquad (2)$$
$$+\dot{m}_w C_{pw}\left(T_{w,\,in}-T_{w,out}\right)$$

where, δ is either 0 or 1 depending whether the adsorbent bed is working as desorber or adsorber and γ is either 1 or 0 depending on whether the bed is connected with evaporator or another bed.

The heat transfer and energy balance equations for evaporator can be expressed as:

$$T_{chill,\,out}=T_{eva}+\left(T_{chill,\,in}-T_{eva}\right)\exp\left(-\frac{U_{eva}A_{eva}}{\dot{m}_{chill}C_{p,chill}}\right) \qquad (3)$$

$$\frac{d}{dt}\left\{\left(W_{eva,w}C_{pw}+W_{eva}C_{p,eva}\right)T_{eva}\right\}=-L\,W_s\frac{dq_{ads}}{dt}$$
$$-W_s C_{pw}\left(T_{cond}-T_{eva}\right)\frac{dq_{des}}{dt} \qquad (4)$$
$$+\dot{m}_{chill}C_{p,chill}\left(T_{chill,\,in}-T_{chill,out}\right)$$

The heat transfer and energy balance equations for condenser can be written as:

$$T_{cond,\,out}=T_{cond}+\left(T_{cw,\,in}-T_{cond}\right)\exp\left(-\frac{U_{cond}A_{cond}}{\dot{m}_{cw}C_{pw}}\right) \qquad (5)$$

$$\frac{d}{dt}\left\{\left(W_{cw,w}C_{pw}+W_{cond,hex}C_{p,cond}\right)T_{cond}\right\}=$$
$$-L\,W_s\frac{dq_{des}}{dt}-W_s C_{p,w}\left(T_{des}-T_{cond}\right)\frac{dq_{des}}{dt}$$
$$+\dot{m}_{cw}C_{pw}\left(T_{cw,\,in}-T_{cw,out}\right) \qquad (6)$$

The mass balance for the refrigerant can be expressed as:

$$\frac{dW_{eva,w}}{dt}=-W_s\left(\frac{dq_{des-cond}}{dt}+\frac{dq_{eva-ads}}{dt}\right) \qquad (7)$$

where, the subscripts *des-cond* and *eva-ads* stand for the vapor flow from desorber to condenser and evaporator to adsorber, respectively.

4. MEASUREMENT OF THE SYSTEM PERFORMANCE

The performance of a three-bed adsorption chiller with mass recovery is mainly characterized by cooling capacity (CC) and coefficient of performance (COP) and can be measured by the following equations:

Cooling Capacity (CC) =

$$\frac{\dot{m}_{chill}C_w\int_0^{t_{cycle}}\left(T_{chill,in}-T_{chill,out}\right)dt}{t_{cycle}}$$

Coefficient of Performance (COP) =

$$\frac{\dot{m}_{chill}\,C_w\int_0^{t_{cycle}}\left(T_{chill\,,in}-T_{chil\,,out}\right)dt}{\dot{m}_{hot}\,C_w\int_0^{t_{cycle}}\left(T_{hot,in}-T_{hot,out}\right)dt}$$

5. RESULTS ANDDISCUSSION

In the present analysis, a cycle simulation computer program is developed to predict the performance of the three-bed chiller with mass recovery. The systems of differential equations (1)-(7) are solved by finite difference approximation with a time step 1 sec. In the numerical solution of the differential equations, successive substitutions of the newly calculated values were used, with the iterative loop repeating the calculations until the convergence test is satisfied. The convergence factor for all parameters of the present study will be taken as 10^{-3}.

The base line parameters and standard operating conditions for the chiller operation are listed in Table 2 and Table 3, respectively.

TABLE 2 BASELINE PARAMETERS

Symbol	Value	Unit
A_{hex}	1.45	m^2
A_{eva}	0.665	m^2
A_{con}	0.998	m^2
C_{ps}	924	J/kg.K
C_{pw}	4.18E+3	J/kg.K
$C_{p,chill}$	4.20E+3	J/kg.K
D_{so}	2.54E-4	m^2/s
E_a	2.33E+3	J/kg
L	2.50E+6	J/kg
Q_{st}	2.80E+6	J/kg
R	4.62E+2	J/kg.K
R_p	0.35E-3	m
U_{ads}	1380	$W/m^2{\cdot}K$
U_{des}	1540	$W/m^2{\cdot}K$
U_{eva}	3550	$W/m^2{\cdot}K$
U_{cond}	4070	$W/m^2{\cdot}K$
W_s	14(for bed1 & bed2), 7 for bed3	kg
W_{cw}	5	kg
$C_{p,cu}$	386	J/kg.K
$C_{p,Al}$	905	J/kg.K
W_{khex}	12.67	kg
W_{fhex}	5.33	kg
$W_{eva,w}$	25	Kg

TABLE 3
STANDARD OPERATING CONDITION

	Temperature [ºC]	Flow rate (kg/s)
Hot water	50 ~ 65	0.4
Cooling water	30	0.74[=0.4(ads)+0.34(cond)]
Chilled water	14	0.11
Cycle Time	2400s=(1100 ads/ des+40 mr+30ph+30pc) s×2	

5.1 EFFECT OFDIRIVING HEAT SOURCE TEMPERATURE ON CC AND COP

Fig.2 and Fig.3 shows the effect of heat source temperature on COP and cooling capacity of the proposed system. From Fig.3, it is clearly found that COP of the cycle with mass recovery is higher than that of the cycle without mass recovery if heat source temperature is 65^0 C. Cooling capacity of each cycle increases as the heat source temperature increases. It should be noted that the cooling capacity (CC) of the proposed cycle with mass recovery is much better than that of the proposed cycle without mass recovery (see Fig.2) in the range of heat source temperature from 50^0C to 65^0 C.

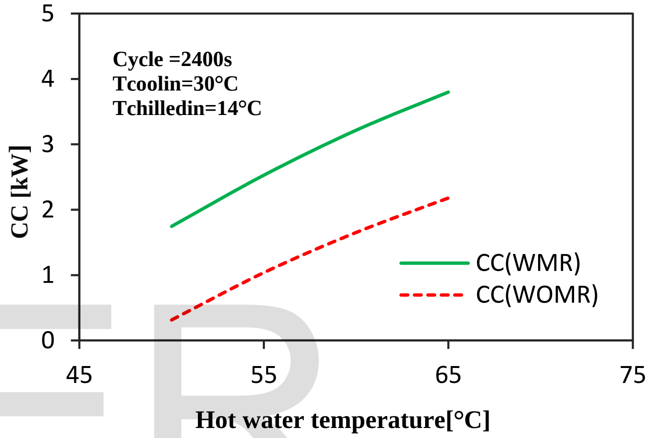


Fig.2.The effect of heat source temperature on CC

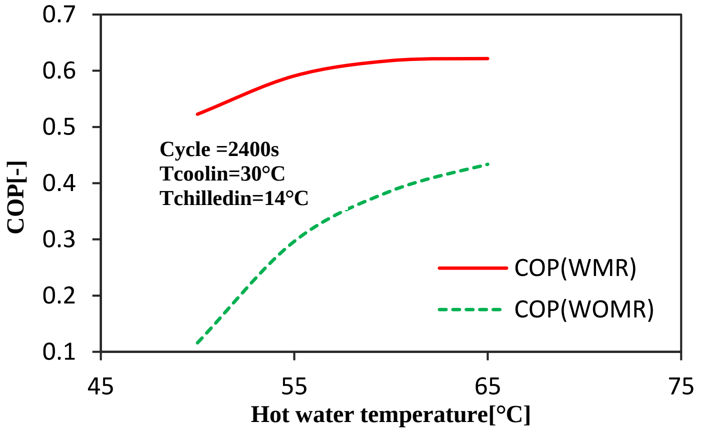


Fig. 3.The effect of heat source temperature on COP

5.2 EFFECT OF COOLING SOURCE TEMPERATURE ON CC AND COP

Fig.4 and Fig.5 show the effect of cooling water inlet temperatures on CC and COP, respectively. In the present simulation, cooling water mass flow rate into adsorber is taken as 0.4 kg/s, while for the condenser the coolant mass flow rate is taken as 0.34 kg/s. The CC increases steadily as the cooling water inlet temperature is lowered from 35 to 20^{0}C. This is due to the fact that lower adsorption temperatures result in larger amounts of refrigerant being adsorbed and desorbed during each cycle. The simulated COP values also increases with lower cooling water inlet temperature. For the three bed chiller the COP value reaches 0.6975 (with mass recovery) and 0.6285 (without mass recover) with 65^{0}C driving source temperature in combination with a coolant inlet temperature of 20^{0}C.

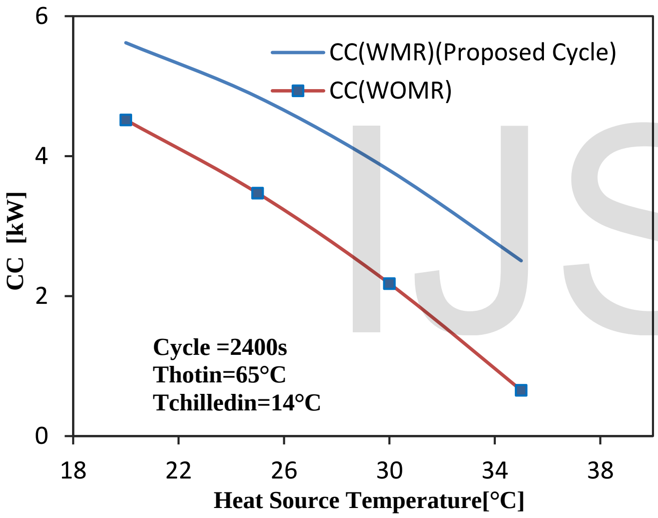


Fig. 4. The effect of cooling water inlet temperature on

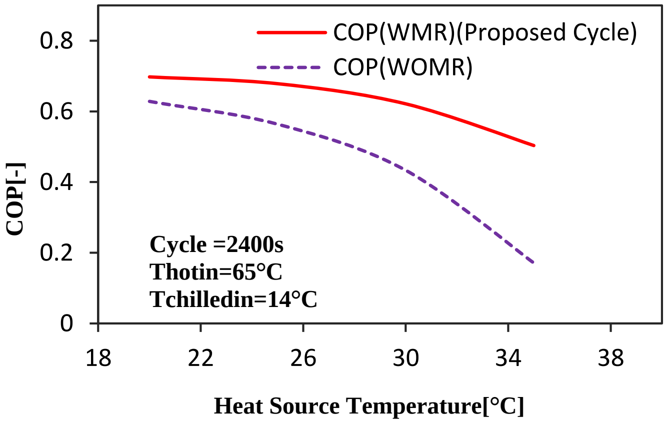


Fig. 5. The effect of cooling water inlet temperature on

5.3 EFFECT OFDRIVING HEAT SOURCE TEMPERATURE ON CHILLED WATER OUTLET TEMPERATURE

The ability to produce a low chilled water outlet is one of the indicators to test the performance of the new cycle. The performance of the proposed cycle with mass recovery is much better than that of the proposed cycle without mass recovery because the chilled water outlet temperature of the proposed cycle without mass recovery is higher than that of the proposed cycle1 with mass recovery as shown in Figure 6. According to Figure 6, the proposed cycle with mass recovery is able to produce chilled water at lower temperature than that of the proposed cycle without mass recovery.

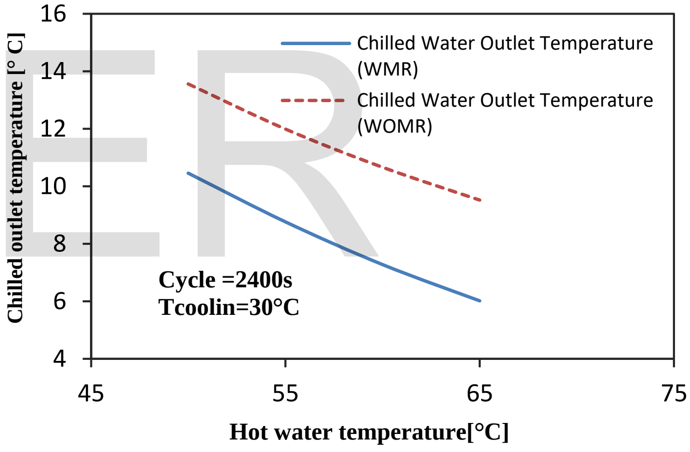


Fig. 6. The effect of heat source temperature on chilled water out outlet temperature

6. CONCLUSION

A novel three-bed chiller (equal bed) with and without mass recovery scheme is proposed and the performances are evaluated by numerical technique. There is an increasing need for energy efficiency and requirement for the system driven with low temperature heat source. The following concluding remarks can be drawn from the present analysis:

i. The main feature of the proposed chiller is the ability to be driven by relatively low temperature heat source. The chiller can utilize the fluctuated heat source temperature between 50^0C to 65^0C to produce effective cooling along with a coolant inlet at 30^0C.

ii. Cooling capacity of the proposed chiller is increased as heat source temperature is increased from 50^0C to 65^0C and cooling water inlet temperature is decreased from 40^0C to 20^0C.

iii. The optimum COP value (0.6214) is obtained for hot water inlet temperature at 65^0C in combination with the coolant and chilled water inlet temperatures are 30^0C and 14^0C, respectively. The delivered chilledwater temperature is obtained at 6.0148^0C.

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